

Evaluating the Adsorption of Reactive Red Dye Using Natural Zeolite: The Role of Solution Aging

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Abstract Reactive dye pollution is a major environmental problem in the textile industry. The study investigated the impacts of dye aging on the adsorption of reactive red dye using the natural zeolite. The natural zeolite was characterized by various methods, including X-ray fluorescence (XRF) and Fourier-transform infrared spectroscopy (FT-IR), X-ray diffraction (XRD), and Raman spectroscopic analysis. The pH and absorbance of the dye solutions were affected by the aging of the dye solutions, which led to a decrease in removal efficiency and adsorption capacity as aging progressed. The results showed that fresh dye solutions were adsorbed more efficiently than aged dye solutions, and the Freundlich isotherm showed the best fit to the experimental data. It indicates that the adsorption took place on the heterogeneous surface of the zeolite. The results suggest that the history of the dye solutions should be taken into account in adsorption studies for better remediation strategies.

Keywords Adsorption, Reactive red dye, Natural zeolite, Time-dependent transformations, Aging

1. Introduction

Reactive dyes, particularly reactive red dye, form covalent bonds with textile fibers but can be hazardous when released into wastewater. They have high solubility, color permanence, and resistance to biodegradation, leading to significant chemical oxygen demand (COD) and potential toxicity in aquatic environments [1], [2]. Conventional treatment methods are often ineffective, prompting interest in natural zeolite as a cost-effective and eco-friendly adsorbent due to its porous structure and ion exchange capacity [3]. Additionally, reactive dye solutions undergo physicochemical changes during storage, affecting their stability and adsorption capabilities [4]. Understanding the impact of dye aging on adsorption is crucial for improving wastewater treatment systems designed for stored dye effluents.

2. Materials and Methods

2.1. Chemicals and Reagents

This study used Reactive Red 120 dye as an adsorbate. pH was adjusted with analytical grade 0.1 M hydrochloric acid (HCl) and 0.1 M sodium hydroxide (NaOH). Dye solutions were prepared with deionized water. Natural zeolite (clinoptilolite) was used as an adsorbent in the adsorption

studies. All reagents were used without further purification.

2.2. Characterization of the Natural Zeolite

Adsorbent characterization is crucial in adsorption studies as it correlates the material's structure with its performance. In this section, the main properties related to the study of the retention mechanisms and the interaction of surfaces of adsorbents and pollutants are described. The natural zeolite was characterized using XRF, XRD, FT-IR, and Raman spectroscopy.

2.3. Preparation and Aging of Dye Solutions

A stock solution of reactive red dye at 1000 mg/L was prepared using deionized water and then diluted to create a 100 mg/L working solution for aging and adsorption experiments. Five 200 mL aliquots were stored in amber glass bottles to reduce light exposure. These solutions were aged for different durations: 0 hours, 24 hours, 72 hours, 7 days, and 14 days, to evaluate their effects on physicochemical properties and adsorption behaviours. The analysed parameters included pH and absorbance at 540 nm, which were monitored for changes that could indicate hydrolysis, molecular aggregation, and potential degradation [5]. All results were obtained in triplicate to ensure accuracy and reproducibility.

2.4. Batch Experiments

2.4.1. Effect of Solution pH on the Adsorption of Reactive Red Dye

The effect of solution pH (3, 5, 7, and 9) on the dye

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adsorption was tested by employing 0.5 g of natural zeolite in a 100 mg/L dye solution and shaking at 150 rpm for 120 minutes. The mixtures were filtered, and the dye concentration after equilibration was evaluated by UV-visible spectrophotometry at 540 nm. The experiment examined the effect of pH on surface charge, dye speciation, and the overall adsorption efficiency of zeolite [6].

2.4.2. Effect of Initial Dye Concentration on the Adsorption of Reactive Red Dye

All studies under this parameter were carried out at constant dye concentrations (50 mg/L, 75 mg/L, 100 mg/L, 125 mg/L, and 150 mg/L), an agitation speed of 150 rpm, room temperature, and a pH of 7.0. 5g zeolite adsorbent was added to a 250 mL flask holding 100 mL dye solution and agitated to ensure thorough dispersion, and filtered after equilibration. The residual dye was measured using a UV-visible spectrophotometer at 540nm, which facilitated the analysis of the adsorption capacity and isotherm data [6].

2.4.3. Effect of Adsorbent Dose on Adsorption of Reactive Red Dye

The effect of adsorbent dose was examined by varying the dose from 0.5g, 0.75, 1g and 2.0 g at a constant dye concentration of 100 mg/l in solution. The mixtures were shaken for 120 minutes at 150 rpm at room temperature. After achieving equilibrium, the suspensions were filtered, and the residual dye was quantified using a UV-visible spectrophotometer. The percentage dye removal and the adsorption capacity (q_e , mg/g) were measured in triplicate [6].

2.4.4. Effect of Contact Time on Adsorption of Reactive Red Dye

Adsorption contact time was determined by shaking 0.5 g of natural zeolite with 100 mL of 100 mg/L dye at room temperature, pH 7, and 150 rpm. Samples were filtered for 5, 15, 30, 60, 120, and 180 minutes before being analyzed using a UV-visible spectrophotometer. The percentage dye removal and the adsorption capacity (q_e , mg/g) were measured in triplicate.

2.4.5. Effect of Dye Aging Time on the Adsorption of Reactive Red Dye

An aging solution of dye was prepared and evaluated at various time intervals (0, 24, 72 hours, 7 days, and 14 days) under controlled conditions: 0.5 g of adsorbent, 100 mg/L dye concentration, pH 7, and 120 minutes of contact time at room temperature. Each solution was filtered and analyzed using a UV-visible spectrophotometer to assess adsorption efficiency changes over time. This study compares the adsorption of fresh versus aged dye solutions, providing insights into the time effects and behavior of dyes in wastewater treatment processes.

2.5. Adsorption Isotherms

The adsorption data of Reactive Red 120 dye onto zeolite were fitted to the Freundlich and Langmuir isotherm models to study the adsorption behavior and equilibrium characteristics of the adsorption process. The equilibrium dye concentrations were measured using UV-visible spectrophotometry, and the adsorption capacity (q_e) was determined as shown in Equation 1 [7].

$$q_e = \left[\frac{C_0 - C_e}{W} \right] \quad (3.1)$$

where C_0 and C_e (mg/L) represent the initial and equilibrium concentrations of the dye solution, respectively. W (g) is the mass of zeolite, and V is the volume of the solution used (L). Equation 3.2 shows the linearized Freundlich isotherm used in this study.

$$\ln q_e = \ln K_F + \frac{1}{n} \ln C_e \quad (3.2)$$

Where: K_F = Freundlich isotherm constant associated with adsorption capacity, q_e = adsorption at equilibrium, $1/n$ = Heterogeneity index associated with adsorption intensity, C_e = concentration of the zeolite in solution at equilibrium. Equation 3.3 shows the linearized Langmuir adsorption isotherm.

$$\frac{C_e}{q_e} = \frac{C_e}{q_m} + \frac{1}{K_L q_m} \quad (3.3)$$

Where, C_e is the equilibrium dye concentration (mg/L); q_e is the adsorption capacity (mg/g); q_m is the maximum monolayer capacity (mg/g); K_L is the isotherm constant (L /mg) [7].

3. Results and Discussions

3.1. XRF Analysis of the Natural Zeolite

Table 1. Elemental and Oxide Composition of Natural Zeolite

Element/Oxide Name	Mean % of Chemical Composition Mean $\pm$ SD
MgO	0.572 $\pm$ 0.517
Al ₂ O ₃	3.688 $\pm$ 0.226
SiO ₂	88.611 $\pm$ 0.617
P	0.064 $\pm$ 0.022
S	0.105 $\pm$ 0.019
Cl	0.112 $\pm$ 0.026
K ₂ O	0.892 $\pm$ 0.018
Ca	2.284 $\pm$ 0.080
Ti	0.082 $\pm$ 0.012
V	0.002 $\pm$ 0.005
Mn	0.065 $\pm$ 0.005
Fe	3.369 $\pm$ 0.027
Cu	0.007 $\pm$ 0.001
Zn	0.018 $\pm$ 0.002
Nb	0.006 $\pm$ 0.001

SD-Standard deviation

A natural zeolite sample was analyzed by X-ray fluorescence (Bruker 5117) to establish its elemental and oxide composition, as shown in Table 1 above.

Silica (SiO_2) predominated, accounting for 88.611 %, indicating an aluminosilicate structure and favourable adsorption properties. Aluminium oxide (Al_2O_3) is identified at 3.688 %, reflecting aluminium in the framework. The $\text{SiO}_2/\text{Al}_2\text{O}_3$ ratio of 24.03 indicates a silica-rich zeolite, which is stable, hydrophobic, and chemically resistant, making it excellent for adsorbent applications in eliminating organic contaminants. Other elements include iron (Fe) at 3.369 %, calcium (Ca) at 2.284 %, and potassium oxide (K_2O) at 0.892%. Trace elements, such as magnesium oxide (MgO) at 0.572 %, show a predominance of silica and alumina, which is necessary for a porous structure and ion exchange. These characteristics improve adsorption due to the existence of active sites and electrostatic interactions with pollutants in aqueous solutions [8], [9].

3.2. X-ray diffraction analysis (XRD)

X-ray diffraction (D6 phaser) analysis was carried out to determine the crystalline phases and mineralogical composition of the natural zeolite sample.

The crystallinity and mixed zeolitic phases of natural

zeolite were confirmed through X-ray diffraction (XRD) analysis, which revealed several distinct diffraction peaks. Notable findings include the dominant clinoptilolite/heulandite phases associated with specific peaks, such as ($2\theta = 15^\circ$). An additional peak at 19° indicates the presence of clinoptilolite/heulandite and potentially mordenite phases. Reflections at (9.8° ; 11.7° ; 22.4° ; 26.0° ; 29.9° ; and 32.3°) provide additional evidence for the existence of clinoptilolite [10]. Higher-angle reflections at 50° ; 60° ; 66° ; and 71° were also employed to identify other mixed zeolite phases, including mordenite, chabazite-Ca, and analcime [11]. These results underscore the crystalline structure and structural heterogeneity of natural zeolite, which is significant due to its porous nature that facilitates dye removal in water treatment applications.

3.3. FT-IR Analysis

The FT-IR analysis identified key functional groups and structural vibrations in natural zeolite, confirming the presence of hydroxyl groups, adsorbed water, and the aluminosilicate framework related to its adsorption properties. Figure 2 shows the FT-IR spectrum, displaying characteristic absorption peaks that correspond to different vibrational modes of the zeolitic framework.

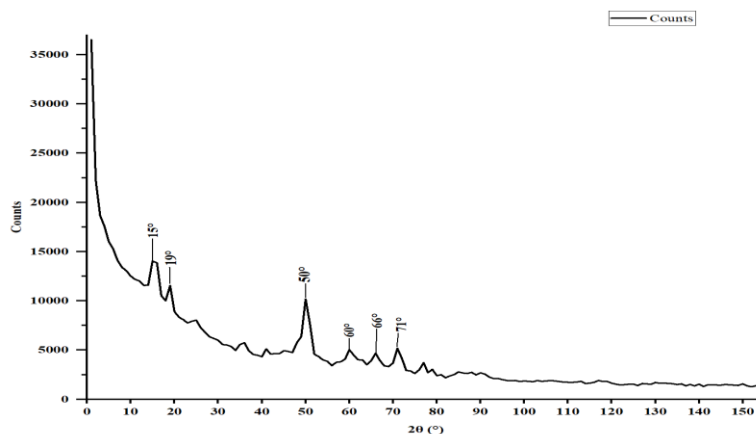


Figure 1. X-ray diffraction pattern of natural zeolite showing the crystalline phases and mineral composition before adsorption

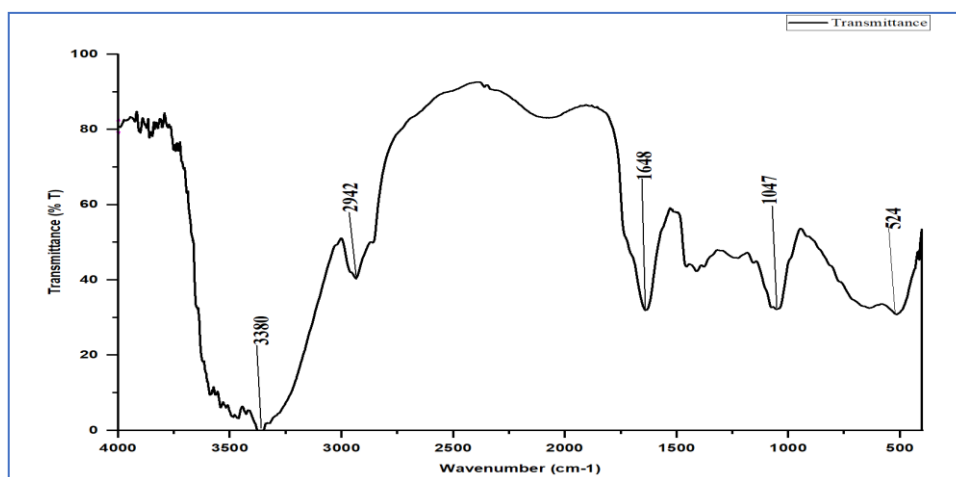


Figure 2. FT-IR spectrum of the natural zeolite showing the major functional groups and characteristic aluminosilicate framework vibrations

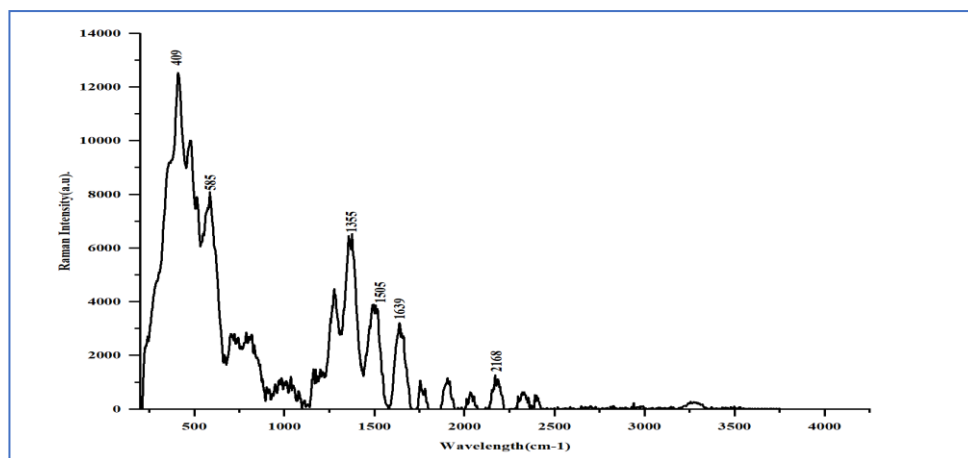


Figure 3. Raman spectrum of natural zeolite showing major structural vibration bands

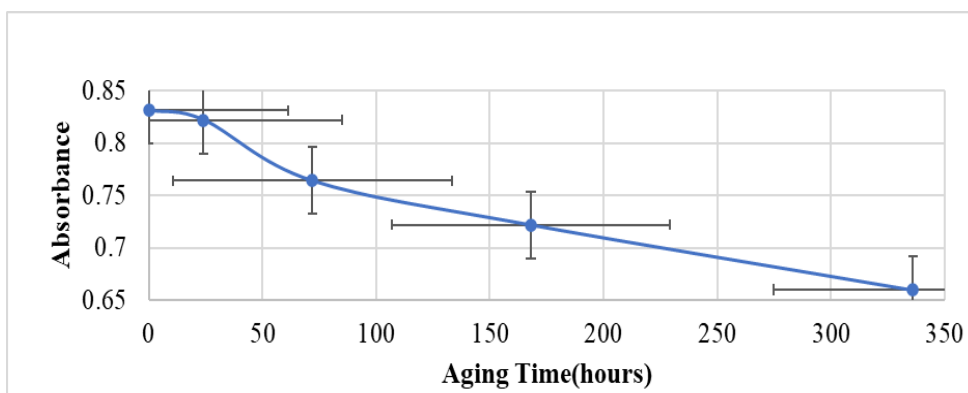


Figure 4. Effect of dye aging time on absorbance of reactive red dye

The FT-IR spectrum of natural zeolite revealed key peaks at 3380, 2942, 1648, 1047, and 524 cm^{-1} , indicating its functional groups and structural vibrations. The peak at 3380 cm^{-1} corresponds to O–H stretching vibrations of hydroxyl groups and bound water, crucial for offering adsorption sites for reactive dye molecules. The 1648 cm^{-1} band relates to H–O–H bending vibrations of water in zeolite pores, confirming its hydrated and porous nature, which aids dye retention [12]. A prominent 1047 cm^{-1} absorption signifies Si–O–Si and Al–O–Si bond stretching, essential for explaining ion exchange and adsorption behaviors in dye removal [13]. The 524 cm^{-1} peak indicates T–O bending vibrations, ensuring the integrity of the zeolite's crystal structure, while the weak 2942 cm^{-1} band suggests minor C–H stretching from surface impurities that may influence adsorption processes [12].

3.4. Raman Spectroscopic Analysis

Raman spectroscopy (ATR3000-785) was used to identify the structural vibrations and the mineralogical features of the natural zeolite. The analysis was used to confirm the framework-related vibrational bands of the zeolite aluminosilicate structure as shown in Figure 3 above.

From figure 2 shown above, natural zeolite exhibits Raman peaks at 409, 585, 1355, 1505, 1639, and 2168 cm^{-1} . The 409 cm^{-1} band confirms the presence of zeolite T–O–T

framework vibrations, which are essential for adsorption. The 585 cm^{-1} band linked with T–O bending vibrations suggests structural integrity, which is important for dye adsorption. Bands at 1355 and 1505 cm^{-1} may be contaminants, indicating the natural zeolite's heterogeneous mineral phase. The 1639 cm^{-1} band corresponds to H–O–H bending vibrations from adsorbed water, which influence dye molecule uptake. The faint 2168 cm^{-1} band is most likely caused by pollutants and should be treated with caution [14]. Overall, the Raman spectrum confirms the findings of the FT-IR and XRD analyses, emphasizing the zeolite's features crucial to dye removal, such as pore accessibility and electrostatic interactions [15].

3.5. Effects of Dye Aging Time on Physicochemical Characteristics of Reactive Red Dye

Aged Reactive Red dye solution was evaluated for 0 hours, 24 hours, 72 hours, 7 days, and 14 days to study the impact of storage time on its physicochemical properties before adsorption. Key parameters such as pH and absorbance were measured under laboratory conditions to evaluate potential changes that could influence the dye's adsorption efficiency on natural zeolite. Figures 4 and 5 show the effects of aging time on absorbance and pH, respectively.

Figure 4 illustrates that the absorbance of Reactive Red dye declines from 0.831 (0 hours) to 0.660 (after 14 days),

indicating reduced dye intensity due to storage. The gradual decrease suggests a reduction in the concentration or activity of absorbable species over time. Initial slight changes occur within the first 24 hours, followed by significant modifications from 72 hours to 14 days, implying time-dependent physicochemical alterations such as dye hydrolysis, molecular aggregation, and degradation [16]. These aging processes affect the dye's stability and its adsorption properties on natural zeolite, as aged dye molecules may interact differently with adsorption sites compared to fresh solutions.

As shown in Figure 5 below, the reactive red pH drops from 6.80 to 5.90 over 14 days which suggests more acidity during aging. This points to physicochemical processes such as hydrolysis, aggregation, and degradation processes producing hydrolyzed species and intermediates with acid characteristics [17]. The dissociation of functional groups in the dye structure also increases hydrogen ions, altering the solution's stability [18]. This pH decline correlates with reduced absorbance, highlighting the adverse effects of aging on the dye's physicochemical and adsorption properties on natural zeolite.

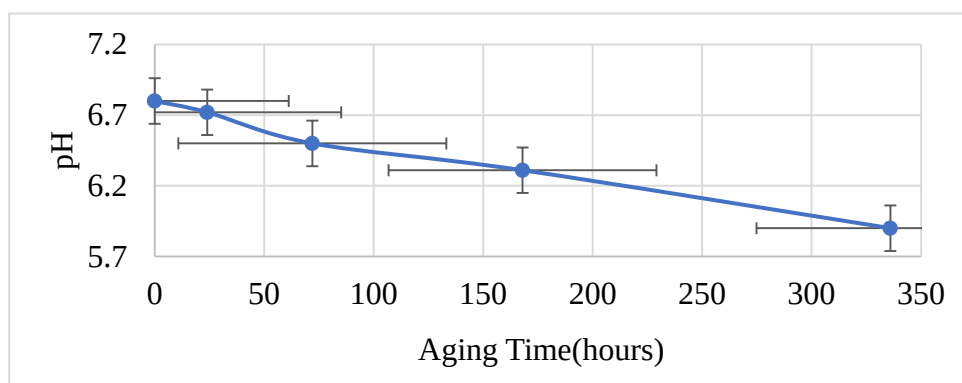


Figure 5. Effect of Dye Aging Time on pH of Reactive Red Dye Solution

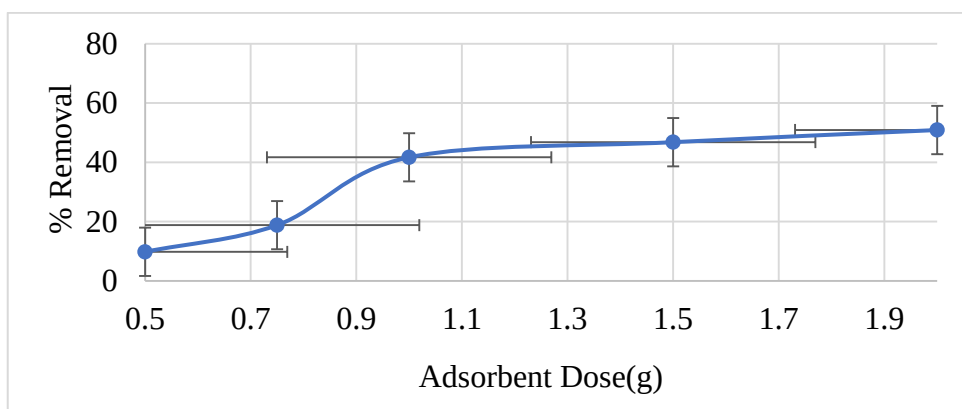


Figure 6. Effect of Adsorbent dose on percentage removal of natural zeolite

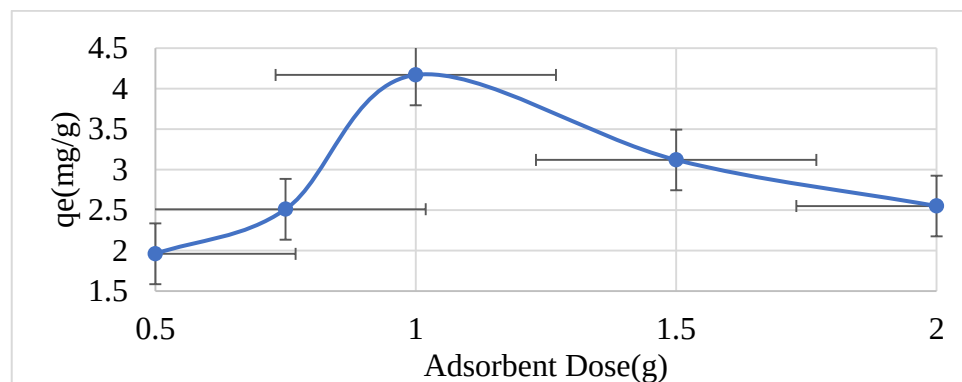


Figure 7. Effect of Adsorbent dose on adsorption capacity of natural zeolite

3.6. Effect of Adsorbent Dose

The study examined how varying the dosage of natural zeolite adsorbent (0.5 g to 2.0 g) affects the percentage removal and adsorption capacity of reactive red dye, as shown in Figures 6 and 7, respectively.

From the data presented in Figure 6, it is evident that the removal percentage of the reactive dye improves with increasing adsorbent dosage. This improvement is primarily due to a rise in the number of available adsorption sites as more natural zeolite is introduced into the dye solution. At lower doses (0.5 g), there are fewer active sites, resulting in higher residual dye concentrations. Other studies corroborate this observation, indicating that a higher adsorbent dosage enhances the number of adsorption sites, leading to greater dye removal through increased surface area for interaction. As the dosage escalates, a marked decrease in equilibrium dye concentration occurs, demonstrating elevated dye removal efficiency linked to augmented surface availability and

adsorption capacity. However, it is noted that excessively high doses may lead to diminishing returns in removal efficiency, as site overlap or full coverage of the adsorbents can occur, limiting further adsorption effectiveness [19], [20].

Figure 7 illustrates that the adsorption capacity (q_e) increases with adsorbent dosage, peaking at 1.0 g due to a higher availability of adsorption sites and enhanced interaction with dye molecules. Beyond this point, however, the adsorption capacity declines as the dosage increases. This decrease is typically observed in adsorption systems, attributed to particle aggregation at higher dosages, which leads to overlapping adsorption potentials. Additionally, at elevated dosages, the concentration of dye molecules in the solution decreases significantly relative to the number of adsorption sites, resulting in reduced dye uptake per unit mass of adsorbent. Similar trends have been noted in studies on dye removal using natural and low-cost adsorbents [20].

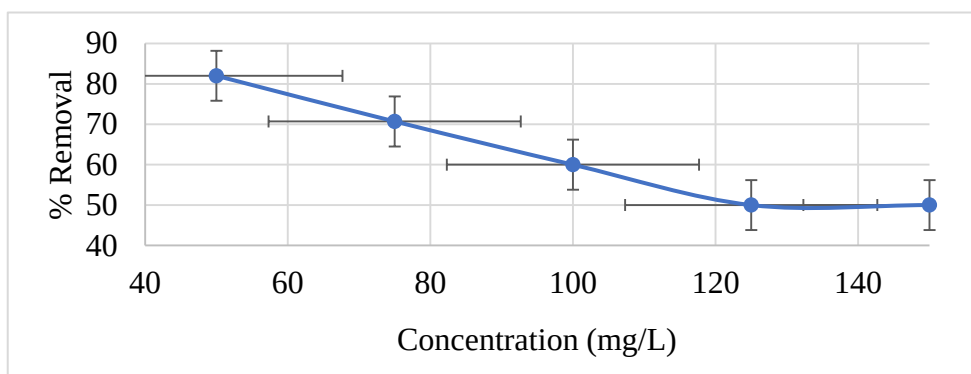


Figure 8. Effect of initial dye concentration on percentage removal of reactive red dye

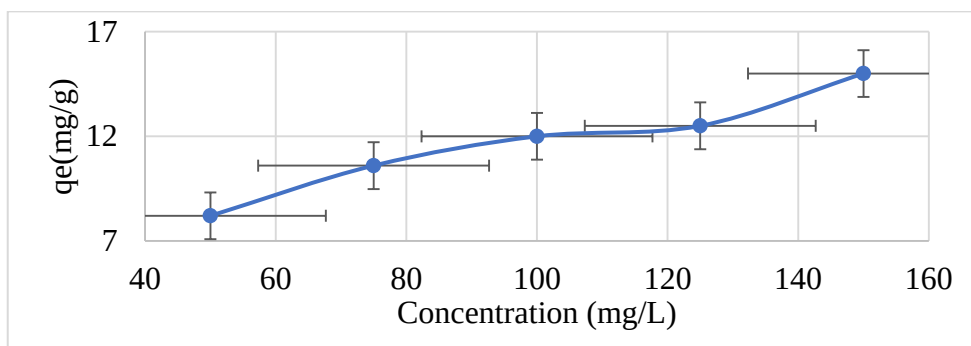


Figure 9. Effect of initial dye concentration on the adsorption capacity of reactive red dye

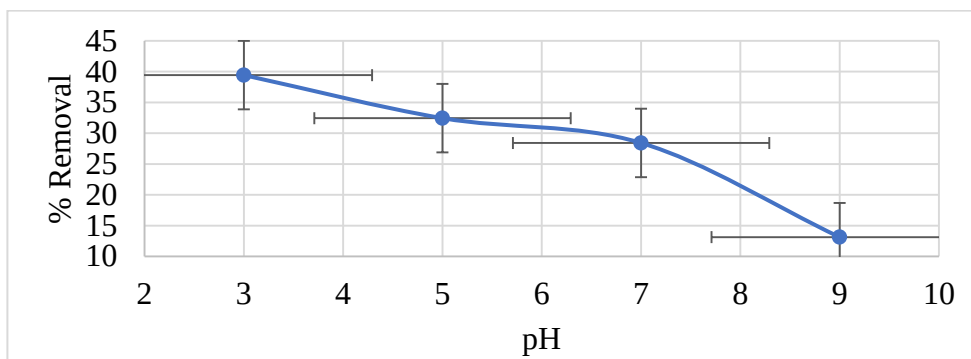


Figure 10. Effect of solution pH on percentage removal of reactive red dye

3.7. Effect of Initial Dye Concentration

The adsorption of reactive red dye on natural zeolite was studied at various concentrations. Results summarized in Figures 8 and 9 illustrate how different concentrations of reactive red dye influenced the percentage removal and adsorption capacity of natural zeolite, respectively.

As the dye concentration increases, the percentage removal of dye significantly decreases due to a limited number of adsorption sites available. At lower concentrations (50 mg/L), the high ratio of adsorption sites to dye molecules allows for maximum adsorption efficiency. However, as concentration rises to 150 mg/L, more dye molecules compete for the same sites, leading to a drop in removal efficiency to 50% at 150 mg/L. This trend indicates saturation of the zeolite surface, as higher concentrations result in more dye than can be effectively adsorbed. Observations from other studies confirm that natural zeolites are more efficient at lower dye concentrations, with 50 mg/L identified as the optimal concentration for maximum removal efficiency [19].

The adsorption capacity (q_e) increases with higher initial dye concentrations, rising from 50 mg/L to 150 mg/L. This increase is attributed to a greater concentration gradient between the dye solution and zeolite, enhancing adsorption. Although the percentage dye removal decreased at higher concentrations, the total dye adsorbed per gram of zeolite

increased due to the greater availability of dye molecules. Supporting results from Hammood *et al.* [6] indicate that increased initial dye concentrations generally enhance adsorption capacity, driven by improved mass transfer, despite potential saturation of adsorption sites.

3.8. Effect of Solution pH

The study investigated how solution pH (3, 5, 7, and 9) affects the adsorption of Reactive Red dye by natural zeolite. Results for equilibrium concentration, percentage removal, and adsorption capacity were determined, with findings detailed in Figures 10 and 11.

Figure 10 shows how solution pH affects the adsorption of Reactive Red dye on natural zeolite. The highest removal percentage was at pH 3 (39.43%), followed by pH 5 (32.44%), pH 7 (28.42%), and pH 9 (13.13%). Lower pH enhances adsorption due to protonation of active sites on zeolite, increasing electrostatic attraction with negatively charged dye molecules. As pH increases, hydroxyl ions compete for adsorption sites, and deprotonation reduces positive charge density, leading to decreased dye removal efficiency. This trend aligns with similar studies on anionic dyes, confirming that an acidic environment is optimal for dye adsorption with natural zeolite, due to less competition from hydroxyl ions [21]. In summary, a lower pH facilitates superior interaction and adsorption of Reactive Red dye onto natural zeolite.

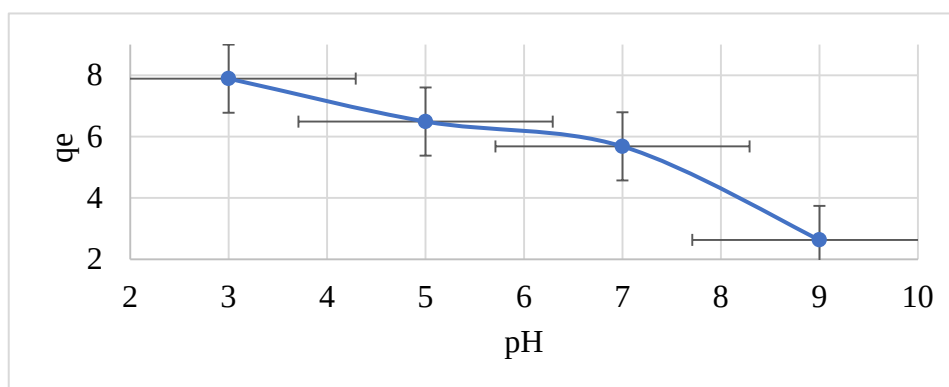


Figure 11. Effect of solution pH on the adsorption capacity of reactive red dye

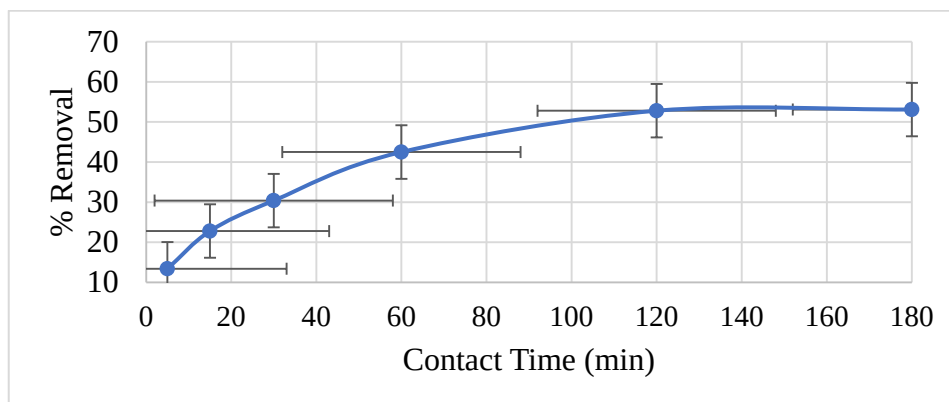


Figure 12. Effect of contact time on percentage removal of reactive red dye

The adsorption capacity of natural zeolite for Reactive Red dye is highest at pH 3 and decreases with increasing pH, indicating that acidic conditions enhance adsorption. This is attributed to the protonation of zeolite surface sites, which attracts negatively charged dye molecules. As pH rises, competition from hydroxyl ions increases, reducing the positive charge on zeolite and weakening the attraction to the dye, leading to lower adsorption capacity. The study aligns with previous findings, confirming that adsorption efficiency diminishes in alkaline environments. The results underscore a linear dependence of zeolite's adsorptive ability on pH, with optimal conditions occurring under acidic conditions [21].

3.9. Effect of Contact Time

The study examined the impact of contact time on the adsorption of Reactive Red dye using natural zeolite over intervals of 5, 15, 30, 60, 120, and 180 minutes. Results on percentage removal and adsorption capacity were detailed in Figures 12 and 13.

Figure 12 shows that the removal percentage of reactive red dye increases with longer contact times, particularly sharp in the first 60 minutes, followed by a gradual rise towards equilibrium at 120 minutes. Beyond this point, no significant increase in removal is observed, indicating saturation of available active sites on natural zeolite. Initially, vacant sites allow rapid dye attachment, but as they fill, the adsorption rate slows due to reduced mass transfer driving force. This behavior parallels that of anionic textile dye adsorption, where initial rapid uptake levels off once saturation occurs [22].

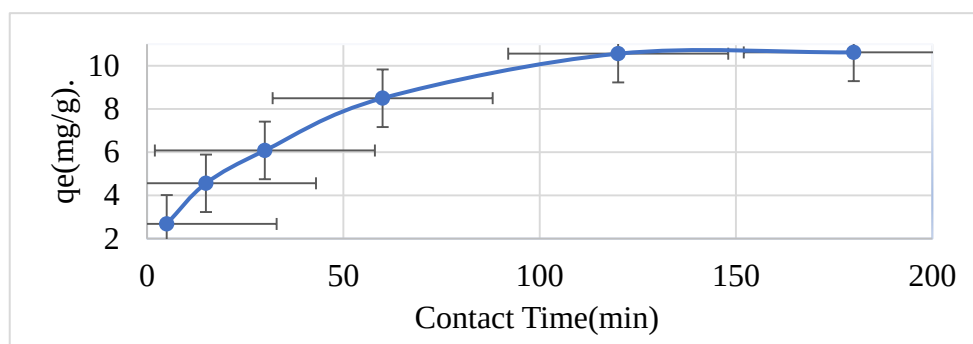


Figure 13. Effect of contact time on the adsorption capacity of reactive red dye

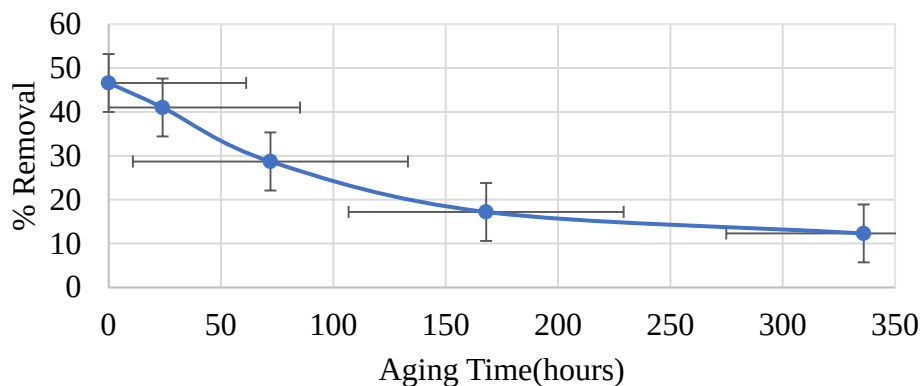


Figure 14. Effect of aging time on percentage removal of reactive red dye

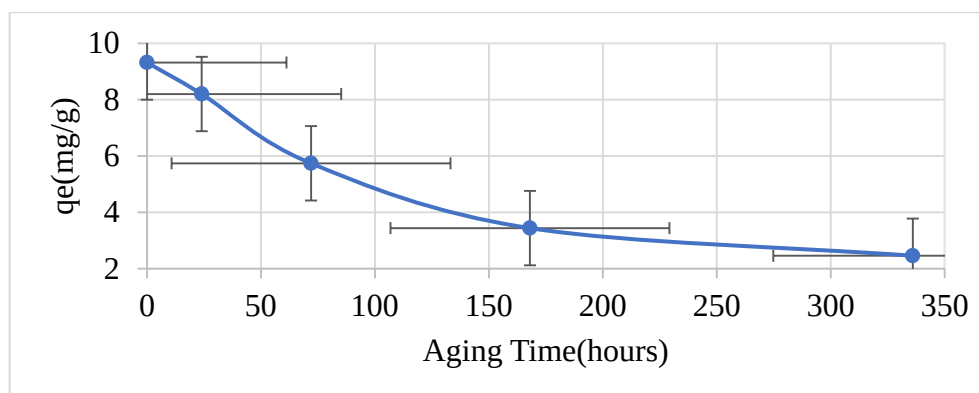


Figure 15. Effect of dye aging time on the adsorption capacity of reactive red dye

Table 2. Langmuir and the Freundlich isotherm parameters for the adsorption of reactive red dye onto natural zeolite

Sorbent	Freundlich			Langmuir		
	1/n	K _F (mg/g)	R ²	K _L (L/mg)	Q _{max} (mg/g)	R ²
Natural zeolite	0.2531	4.73	0.9502	0.01089	11.45	0.9131

1/n=heterogeneity index, K_F=Freundlich constant, R²=correlation coefficient, K_L=Langmuir constant, Q_{max}=adsorption capacity

As illustrated in Figure 13, the adsorption capacity (q_e) of Natural Zeolite for Reactive Red dye increased with contact time, showing significant uptake in the first 60 minutes, after which the rate slowed, indicating occupied adsorption sites. After 120 minutes, no further increase in capacity was observed, signifying that adsorption equilibrium was achieved. The results underscore the importance of adequate contact time for effective dye molecule diffusion to the zeolite's surface, typical of porous natural adsorbents. Therefore, 120 minutes is identified as the optimum time for maximum dye adsorption in the conditions examined.

3.10. Effect of Dye Aging Time

The study investigated the effect of dye aging time on the adsorption of Reactive Red dye onto natural zeolite at 0 hours, 24 hours, 72 hours, 7 days, and 14 days. The effects of dye aging time on percentage removal and adsorption capacity (q_e) were calculated and presented in Figures 14 and 15, highlighting the impact of dye aging on the adsorption efficiency of reactive red dye on natural zeolite.

Figure 14 illustrates the impact of aging time on the removal efficiency of Reactive Red dye using natural zeolite. The highest dye removal was 46.6% at 0 hours, decreasing to 12.3% after 14 days. A significant drop in efficiency occurred within the first 72 hours, likely due to physicochemical changes in the dye solution, including degradation and structural alterations, which reduce the adsorption affinity on the zeolite. Recent studies indicate that dye structure and compatibility with adsorbents significantly affect adsorption, emphasizing that fresh dye solutions yield better removal results [23].

The adsorption capacity (q_e) of dye decreases with aging time, highlighting a significant decline from 9.32 mg/g at 0 hours to 2.46 mg/g after 14 days. The reduction is initially sharp within the first 72 hours, followed by a gradual decrease. This decline is attributed to physicochemical changes in the dye, including degradation, aggregation, hydrolysis, and structural changes, which affect molecular size, charge distribution, and functional groups that interact with the zeolite surface. Such changes hinder adsorption efficiency, as similarly noted in literature, with aging and hydrolysis leading to reduced affinity toward adsorbents and restricted accessibility to active sites in zeolite pores [24]. Fresh dye solutions are thus more effective for adsorption processes.

3.11. Adsorption Isotherms

The adsorption isotherms analysis was carried out to describe the interactions between the reactive red dye molecules and the zeolite surface at equilibrium. The Langmuir and the

Freundlich adsorption isotherm models were used to evaluate adsorption behavior, surface characteristics, and suitability for dye removal.

The Freundlich model outperformed the Langmuir model in describing the adsorption of Reactive Red dye onto natural zeolite, with correlation coefficients of $R^2 = 0.9502$ and $R^2 = 0.9131$, respectively. This suggests heterogeneous adsorption sites of varying energies on the zeolite surface. The Freundlich constant ($K_F = 4.73$ mg/g) and a heterogeneity factor ($1/n = 0.2531$) indicate favorable adsorption conditions. The Langmuir model, while also fitting well ($Q_{max} = 11.45$ mg/g), implies that some adsorption occurs in a monolayer on specific active sites. Overall, both models adequately describe the adsorption behavior, with the Freundlich model highlighting the predominant heterogeneous interactions influenced by the zeolite's structural characteristics [25].

4. Conclusions

Natural zeolite effectively removes reactive red dye from aqueous solutions due to its aluminosilicate composition, primarily consisting of 88.611% silica and 3.688% alumina. XRD analysis shows that crystal phases like mordenite enhance its adsorption capacity. Raman and FT-IR analyses confirm the integrity of the zeolite framework. Ageing decreases dye concentration and affects adsorption properties, as shown by a drop in absorbance and pH after 14 days. Optimal dye removal occurs at a zeolite dosage of 1.0 g and lower dye concentrations, with pH 3 favoring adsorption through stronger electrostatic interactions. The Freundlich model fits the adsorption data better than the Langmuir model, indicating a Freundlich constant of 4.73 mg/g and a Langmuir capacity of 11.45 mg/g. This underscores the potential of natural zeolite as a cost-effective and eco-friendly adsorbent for reactive red dye removal from wastewater.

Conflict of Interests

The authors declare that they have no known competing financial interests or personal relationships that could appear to have influenced the work described in this paper.

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